

Modeling Bioelectrochemical Systems for (waste)water Treatment and Bioenergy Recovery with COMSOL

Tolutola Oyetunde, Irina Dana Ofiteru, and Jorge Rodríguez*

Institute Centre for Water and Environmental Research (iWATER)

Masdar Institute of Science and Technology, PO Box 54224, Abu Dhabi, United Arab Emirates

(toyetunde@masdar.ac.ae; iofteru@masdar.ac.ae; jrodriguez@masdar.ac.ae)

Why is this interesting?

Bioelectrochemical systems (BES) are based on the typical electrochemical system (which convert chemical to electrical energy or vice versa) with the inclusion of microbes, serving as catalysts in transferring electrons to/from external electron acceptors (electrodes). They present a unique potential to provide energy-efficient wastewater treatment, utilize organic waste streams to produce energy, and many important chemicals. However, we are a long way from commercial implementations of BES. A key challenge being the poor understanding of the complex phenomena involved.

Our objective

- Investigating the basic chemical, biological and physical phenomena (especially the mechanisms of extracellular electron transfer and the ecology of the microbial communities) that are critical for the performance of BES using COMSOL Multiphysics.
- Model-based technical evaluation of the different BES applications

Modeling strategy

COMSOL-based modeling framework

COMSOL

- Electrochemistry Module**
Model structure validation and parameter calibration by electrochemical techniques (e.g. Electrical impedance spectroscopy, cyclic voltammetry etc.)
- CFD Module**
hydrodynamics of microbial fuel cell (testing different reactor configurations)
- Chemical Reaction Engineering Module**
linking mass, energy and momentum transport with chemical reactions

LiveLink for MATLAB

MATLAB

Code for microbial kinetics and ecology, biofilm dynamics, and electron transfer mechanisms

MATLAB code

EXCEL

Model structure definition: Operating, kinetic, and thermodynamic parameters (to be used in both COMSOL and MATLAB)

LiveLink for Excel

Microbial Model equations

Case study: Simultaneous cathodic reduction of acetate and butyrate to alcohols and simultaneous anodic oxidations of acetate and hydrogen)

$$I_{Acox}^{an} + I_{H2ox}^{an} = I_{an} = I_{obs} \quad I_{Acred}^{ca} + I_{H+red}^{ca} + I_{Bured}^{ca} = I_{ca} = I_{obs}$$

$$E_{Acox}^{Bulk} + \eta_{Acox}^{conc} + \eta_{Acox}^{act} = E_{anode} \quad E_{Acred}^{Bulk} + \eta_{Acred}^{conc} + \eta_{Acred}^{act} = E_{cathode}$$

$$E_{H2ox}^{Bulk} + \eta_{H2ox}^{conc} + \eta_{H2ox}^{act} = E_{anode} \quad E_{Bured}^{Bulk} + \eta_{Bured}^{conc} + \eta_{Bured}^{act} = E_{cathode}$$

$$\eta_{ac-an}^{act} = \frac{KsE \cdot I_{ac-an}}{(I_{ac-max} - I_{ac-an})}$$

$$E_{H+red}^{Bulk} + \eta_{H+red}^{conc} + \eta_{H+red}^{act} = E_{cathode}$$

$$rS_{Acox} =$$

$$q_{ac-e}^{max} \cdot \frac{S_{ac}}{K_s + S_{ac}} \cdot \frac{S_{in}}{K_{in} + S_{in}} X_{ac-e} \cdot I_{ph} \cdot \frac{\eta_{ac}^{act}}{KsE + \eta_{ac}^{act}}$$

Where:

F = Faraday's constant (C/mol_e)

A_{an} = area of anode (m^2)

S_{ac} = conc. of acetate (mol_{ac}/m^3)

S_{in} = conc. of inorganic nitrogen (mol_{in}/m^3)

KsE = half saturation activation overpotential (V)

η_{ac}^{act} = activation overpotential (V)

I_{ph-an} = pH inhibition term (l)

K_s = acetate half saturation constant (mol_{ac}/m^3)

rS_{Acox} = anodic acetate oxidation rate ($mol_{ac}/m^3 \cdot s$)

V_{r-an} = volume of anode compartment (m^3)

Y_e = electron yield per mole of acetate (mol_e/mol_{ac})

q_{ac-e}^{max} = max. specific acetate rate ($mol_{ac}/mol_{ac} \cdot s$)

K_{in} = half saturation for ammonium N (mol_{in}/m^3)

X_{ac-e} = electroactive bacteria conc. (mol_l/m^3)

I_{ac-max} = max. current at perfect electrocatalysis

Electrochemical Techniques

Controlled Potential

Potential Step
Potential sweep (Voltammetry)
Constant Potential (Bulk Electrolysis)

Controlled Current

Chronopotentiometry
Coulometry
Electrolysis

Controlled Charge

Charge step (coulostatic methods)

Impedance methods

AC voltammetry
Electrical Impedance spectroscopy

Expected/ Representative Results

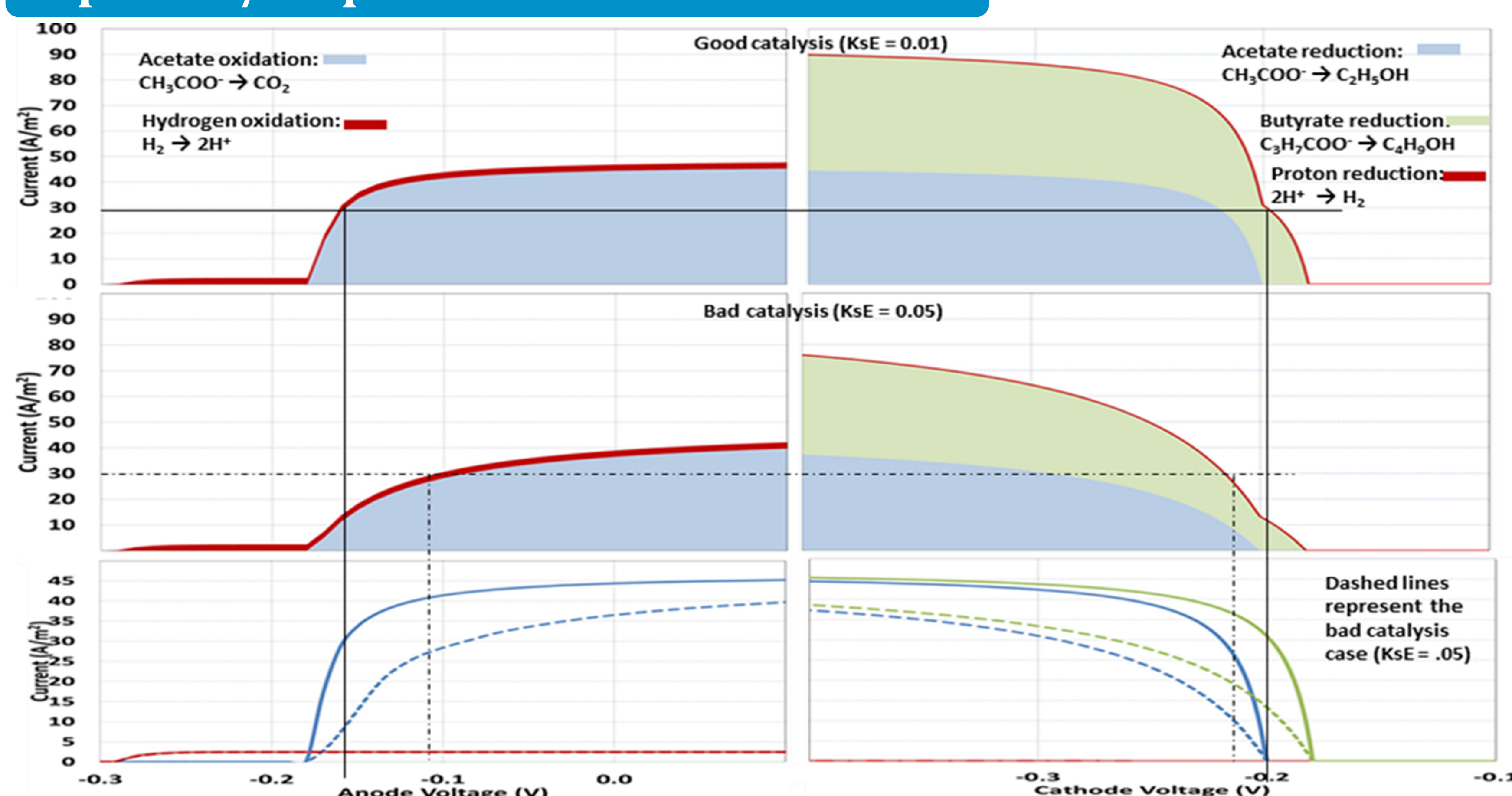


Figure 1. Comparison of potentials and individual current contributions for the simultaneous oxidations of acetate and hydrogen (anode) and reductions of butyrate, acetate and protons (cathode) at two different electrode catalysis efficiencies ($KsE = 0.01$ and 0.05). Arbitrary fixed cathode and anode bulk liquid concentrations of $0.1M$ of butyrate and acetate; $0.3mM$ for dissolved hydrogen and $pH 5$ are used.

Data from Electrochemical experiments

COMSOL-based electrochemical and microbial model

Chemical, biological and physical parameter calibration

Figure 1 shows a representative result for an example time snapshot of bulk concentrations in the case study system. At the bottom, the individual current contributions from each reaction are represented for two different bio-electrode catalysis qualities (KsE values); the top figures represent the aggregated (observed) current values for both cases. Note that electrode potentials are unique for all reactions involved. As an example, in order to achieve the same current ($30 A/m^2$) in the worse catalysis case ($KsE = 0.05 V$), the anode potential has to be placed much higher and the cathode potential much lower requiring more energy supply to make the microbial electrolysis cell process run.

TAKE-HOME INFORMATION

- The proposed model structure provides a platform for elucidating nontrivial interactions between physical, chemical and biological variables using data from classical electrochemical experiments which is critical for commercialization of BES.
- It can be used to perform technical evaluations of BES applications including wastewater treatment, industrial chemical production (bioelectrosynthesis), water desalination and bioremediation etc.

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